RETURN PIPE CAPACITIES											
In Pounds Per Hour											
Pipe	Low Pressure High Pressure Return, Steam Pressure in Psig										
Size	Gravity Vacuum										
In.	Return	Return	25	50	100	150	200	250			
3/4			236	312	419	560	682	1,074			
1	200	350	474	617	823	1,120	1,138	2,150			
1-1/4	400	600	989	1,306	1,755	2,330	2,880	4,450			
1-1/2	700	950	1,610	2,126	2,850	3,800	4,710	7,350			
2	1,200	2,000	3,280	4,325	5,785	7,700	9,550	14,875			
2-1/2	1,650	3,350	5,400	7,160	9,640	12,800	15,850	24,600			
3	2,600	5,350	9,890	13,070	17,550	23,300	28,850	34,750			
4	6,500	11,000	20,800	27,360	36,550	49,200	60,900	73,350			
5	10,400	19,400	38,850	52,925	70,000	91,500	114,500	127,600			
6	18,000	31,000	61,200	83,700	112,700	150,000	185,500	223,100			
NOTES C	ON USE O	F ABOVE	TABLE								
	T I I O(6 - 1				
1	The "Stea	am Pressu	re in PSIG	refers to	the press	ure ahead	of the trap)S			
	which discharge into the return line being sized.										
		deneste is									
2	If the con-	densate is	being coll	ected in a	receiver, a	and then p	umpea				
	back to a	deaerator	or notwell	, the return	n line shou						
	be sized with the use of the tables on page C-1 and C-2.										
2	For the pu	imped roti	Irn systom	mentiona	d in Nota	2 the num	n muet ha	`			
	s For the pumped return system mentioned in Note 2, the pump must be										
a) Return pipe friction from Note 2 above.											
b) Vertical difference in elevation from the level in the condensate receiver											
to the level in the hotwell or deaerator.											
c) The gauge pressure on the surface of the water in the hotwell or deaera											

Table High pressure return

C-6					